GPC Workshop 2022

A comprehensive illustration for Petrobel's experience in evaluating productivity for non-flowing wells using Slug test technique



Presented by Eng. Mostafa Kortam

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FIRST SECTION

Background & Introduction





Welltest Execution

- Typically it is a repeated series of Production and shut-in (2 cycles)
- Usually takes 5-8 days
- Comprise several components;
 - Test string (PKR & Valves).
 - Unloading method such as ; Coild tubing (N2), Swap cups, Downhole valve
 - Surface facility equipment.
 - Rate measurement meters.



Conventional Welltest Outlines

- Constant / stable / accurate production rate.
- Require safe handling of produced fluids.
- Challenged in non-flowing (depleted) wells.

Slug Test Method

- Used mainly in non-flowing (depleted) wells.
- Can be merged with TCP (Underbalance perforation).
- Can be used in hig pressure wells if no flow is desired.

where most of the discrepancy arises. Errors are also undoubtedly introduced by the assumption of the type of fluid entering the drillstring (all mud in the first flow period, all oil in the second flow period). Another possible source of some of the discrepancy may be that part of the production during the first flow period is a result of decompression of the wellbore fluid from hydrostatic mud pressure, about 2,300 psig, to the formation pressure of about 1,700 psig. The over-pressure in and near the wellbore can affect both the flow rate and the pressure during the first flow period. Generally, the results from the second flow period and and should be avoided if possible. Normally, one does not analyze pressure data from the first flow and shut-in periods. Results from analyzing those data tend to be less accurate than results from analyzing the second flow and shut-in periods because of longer flow duration and likely absence of mud production during the second flow period.

Analyzing Flow-Period Data

If rate variation can be estimated during the flow period, it is possible to analyze pressure data from the flow period with methods given in Section 4.2. Such multiple-rate

DRILLSTEM TESTING

analyses can be particularly useful for wells with substantial flowing bottom-hole pressure increase that either do not flow to the surface or have insufficient surface flow time at a stable rate to provide reliable analysis results from the shutin pressure data.

Occasionally, the pressure exerted by the produced fluid column can reach the reservoir pressure, causing production to stop during the flow period — the well kills itself. In such cases, data from the shut-in period cannot be analyzed. However, flow-period data can be analyzed by multiple-rate techniques (Section 4.2) or by type-curve matching techniques presented in Refs. 9 and 14 through 17. The type curves in Refs. 14 through 16 do not consider škin factor, so they are not recommended. Ramey, Agarwal, and Martin⁹ provide type curves that include skin effect that may be used to analyze DST flow-period data *as long as flow does not reach the surface* and there is no significant change in the wellbore storage coefficient (pipe inner diamater). Figs. 8.8A through 8.8C* are the Ramey-Agarwal-Martin type curves. In those figures, the dimensionless pressure ratio is defined as

 $p_{DR} = \frac{p_D}{p_{Do}} = \frac{p_i - p_{wf}(t)}{p_i - p_o} , \qquad (8.12)$

where p₀ is the pressure existing in the drillstring im-*See footnote on Page 24.





Slug Test Scheme



Slug Test Scheme





Slug Test Optained Data



Mostafa Kortam

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Second SECTION





Slug Test Analysis Techniques

- 1. Rough estimation technique using spreadsheet.
- 2. Type curve match.
- 3. Commercial Software.



1. Rough estimation technique using spreadsheet.



Caluclation sheet



FORMATION	KARE	EM									
Date	08-May	/-22									
FILL UP EVALUATION FOR WELL 112-198											
Ps =	1962	Psi Gauge depth =		2519.32	mIVID						
	1443	Psi		2325	MSSL						
D/D cap 19.5 lb/#	0 01776										
Datum	8600	eel	T O Porf		2447	meel					
Ps @ datum	2326	331	Ps@toppe	rfs	2108	nsi	1				
grad	0.365	Psi/ft	Reservoir gra	dient	0.38	psi/ft					
P.I. + 1.5 B	PD/PSI	1									
	PRESS				dV	RATE	PI	AVG PI			
Min.	Psi v		Psi 🔽	ft 🚽	BBI s -		B/D/Psi -	B/D/Ps			
0.0	1443.33	1,000			0000		0.0/1 0	0.0110			
0.5	1459.99	0.968	16.659	45.6412	0.811	2334.49	4.647	4.647			
1.0	1476.35	0.936	16.360	44.8216	0.796	2292.57	4.717	4.682			
1.5	1486.20	0.917	9.845	26.9728	0.479	1379.63	2.898	4.087			
2.0	1496.42	0.898	10.221	28.0017	0.497	1432.25	3.074	3.834			
2.5	1505.94	0.879	9.523	26.0901	0.463	1334.48	2.924	3.652			
3.0	1515.84	0.860	9.902	27.1299	0.482	1387.66	3.108	3.561			
3.5	1526.63	0.839	10.789	29.5600	0.525	1511.96	3.470	3.548			
4.0	1536.56	0.820	9.928	27.2010	0.483	1391.30	3.268	3.513			
4.5	1545.41	0.803	03 8.848 24.241		0.431	1239.92	2.974	3.453			
5.0	1554.16	0.786	786 8.753 23.9796		0.426	1226.53	3.005	3.409			
				//							
81.0	1929.53	0.063	0.470	1.28/1	0.023	65.84	2.008	2.496			
82.0	1929.94	0.062	0.408	1.11/3	0.020	57.15	1.765	2.491			
82.5	1930.35	0.002	0.416	1 1409	0.020	58.36	1.820	2.407			
83.0	1931.18	0.060	0.410	1.1243	0.020	57.51	1.847	2.478			
83.5	1931.57	0.059	0.390	1.0676	0.019	54.60	1.776	2.474			
84.0	1931.98	0.058	0.405	1.1096	0.020	56.76	1.870	2.470			
84.5	1932.36	0.058	0.385	1.0555	0.019	53.99	1.802	2.466			
85.0	1932.76	0.057	0.398	1.0898	0.019	55.74	1.886	2.462			
85.5	1933.14	0.056	0.382	1.0458	0.019	53.49	1.833	2.458			
86.0	1933.53	0.055	0.386	1.0577	0.019	54.10	1.8/9	2.454			
00.5 97.0	1933.90	0.055	0.3/4	1.0255	0.018	52.46	1.646	2.450			
87.5	1934.27	0.054	0.3/1	0.9/89	0.010	48.53	1.000	2.441			
88.0	1934.96	0.053	0.339	0.9299	0.017	47.56	1.732	2 438			
88.5	1935.31	0.052	0.349	0.9563	0.017	48.92	1.811	2.434			
89.0	1935.66	0.051	0.354	0.9707	0.017	49.65	1.862	2.431			

2. Type curve match.

Ps =	1962	Psi						
Po =	1443	Psi						
D.P. size =	5"							
D/P. cap. 19.5 lb/ft	0.01776							
Datum	8600	ssl						
Ps @ datum	2326							
grad.	0.365	Psi/ft						
P.I. <u>+</u> 1.5 BPD/PSI								
TIME (T)	PRESS	PDR						
Min. 👻	Psi 👻	-						
0.0	1443.33	1.000						
0.5	1450.00	0.000						
	1455.55	0.968						
1.0	1476.35	0.968						
1.0 1.5	1435.35 1476.35 1486.20	0.968 0.936 0.917						
1.0 1.5 2.0	1435.35 1476.35 1486.20 1496.42	0.968 0.936 0.917 0.898						
1.0 1.5 2.0 2.5	1435.35 1476.35 1486.20 1496.42 1505.94	0.968 0.936 0.917 0.898 0.879						
1.0 1.5 2.0 2.5 3.0	1435.35 1476.35 1486.20 1496.42 1505.94 1515.84	0.968 0.936 0.917 0.898 0.879 0.860						
1.0 1.5 2.0 2.5 3.0 3.5	1435.35 1476.35 1486.20 1496.42 1505.94 1515.84 1526.63	0.968 0.936 0.917 0.898 0.879 0.860 0.839						
1.0 1.5 2.0 2.5 3.0 3.5 4.0	1435.35 1476.35 1486.20 1496.42 1505.94 1515.84 1526.63 1536.56	0.968 0.936 0.917 0.898 0.879 0.860 0.839 0.820						
1.0 1.5 2.0 2.5 3.0 3.5 4.0 4.5	1435.55 1476.35 1486.20 1496.42 1505.94 1515.84 1526.63 1536.56 1545.41	0.968 0.936 0.917 0.898 0.879 0.860 0.839 0.820 0.803						

 $PD = \frac{Ps - Pi}{Ps - Pc}$

- This method is reliable provided that the density of the fluid is known and the tubing section has a uniform I.D.
- To satisfy the assumption of constant well bore storge.

N.B: After Ramey, Agarwal and Martin.



Caluclation sheet

Fill Up Interpre	etation by T	gpe Curv	after Tep					
<u>Vell Data</u>				<u>Reserv</u>	<u>ioir Dat</u>	a		Vell /Reservoir communication
۲W		3.5	in	Mo		0.35		Measured perf length (m) 6
		0.29	ft	Net pay	(h)	3.5	mts	deviation angle 35.0
Tbg. size		4.5"	in			11.6	ft	N/Giratio 0.7
Tbg. capacity		0.01425	bbl/ft	Poro		12		non perforated interval within body (m) 1.0
Fluid grad.		0.5	Psi/ft	Ct		3.00E-06	1/psi	vertical permeability/Hz permeability ra 0.1
Wellbore storage		0.0005		_				derainage radius / half well spacing /
coeff. (C)		0.0285	DDIrpsi	во		1		boundary limit (m)
Estimated/expect	ed prodirate	1100	bod	Lin rełrw		7.03		derainage Area (lacroe) 7.8
Eponitace are npe ov	ca pros rac		epa	2010				acramager near (aorge)
			Tane Curve M	latch Nata				
curve1				curvel				
Cde^2s	1.00E+05			Cde^2s		2.00E+02		μ C t
tm	10	min		tm		1	min	$K = 3.380 \ \mu \ \cup \ \Box \ \Box \ \Box$
10/CD	0.1667	hrs		10/00		0.0167	hrs	$K = 5.309 \frac{1}{1} \times \frac{1}{1}$
				tD/CD)c	urve	0.0900	hrs	$h t_{M} (U_{D})_{M}$
0.8								
0.8 -								$1 \left[\begin{array}{c} \theta \\ C \\ n \end{array} \right] \left[\begin{array}{c} \theta \\ r \\ m \end{array} \right] \left[\begin{array}{c} 0 \\ 28 \end{array} \right] \\ \left[\begin{array}{c} 0 \\ 28 \end{array} \right] \left[\begin{array}{c} 0 \\ 28 \end{array} \right] \\ \left[\begin{array}{c} 0 \\ 28 \end{array} \right] \left[\begin{array}{c} 0 \\ 28 \end{array} \right] \\ \left[\begin{array}{c} 0 \\ 28 \end{array} \right] \\ \\ \\[\begin{array}{c} $
								$\mathbf{C} = \mathbf{I}_{\mathbf{m}}$
								S = -III
								2 0.89359 C
								-
D.8								
					Cale	ulations		
0.6			2					
					Pern	n. (k)	=[(3389)	"Mo"C"(tD/CD)m)/(h"tm)]
			A DE LE D				15	57 md
0.4			100					
					Shin	(6)	-1/2lo[(c	nhi"C't"rw2"h"(C'de^2z))/(0.89359"C)]
0.8						1 J		
0.2							(0.007)	
					▋		=[0.0070	uo κ njηφυ Μυ (iii(ienwj) ερ
0.1					F.I. 31	(IN	=[0.0070	us K njr(BO MIO (IN(rerrw+s75))
			111.63					00
0.0							12	25
0.01 0.10 0.10	101,00	10.00	o 100.00 10*	10*	effic	iency/		







Third SECTION

Petrobel's Operational Excellence





Improve Well Performances

Clean Perforation tunnel by unplugging the deposit through creating sudden differential pressure would mobilize the clogging material



Formation Heterogeneity Identification

Compare wells producing from same pool and detect underperforming wells & define formation chractristics



Accurate Treatment Judge

Without waiting cleanup post frac treatment and avoiding putting wells on Production test for longer time

Finally !!





Constructing Workflow Strategy



Step 2

• Compare with other Slug tests (offset wells, previous tests)

Step 3

 Calibrate with Surveillance methods (DH sensor, Ecometer pulse, Nodal model match)



Slug test Overall period Build up test (traditional)

Step 1

• Conduct the Slug test

Impact of the application...

• Several advantages can be obtained with utilizing such test.



Effective cost optimization

Safe and simple (no need to manage produced volumes)



















The Role of Wettability in Engineering Operations

Time lapse productivity decline



Caliberation with Buildup









RAM used 894 MB - Free 1114 MB

Slug test in flowing wells (deep)

2090 Psi

Psi

in

bbls/ft

ft ssl

Psi

Psi/ft

1147

3.5

0.00742

9000.0

4182.9

0.560

Ps =

 $P_0 =$

datum

Tbg. size =

Tbg. cabacity =

Ps @ datum

cushion fluid grad.



TIME (T)	PRESS	PDR	dP	dH	dV	RATE
Min. 🖵	Psi 🖵	•	Psi 🖵	ft 🖵	BBL	BBL/C
0.0	1146.8	1.00000				
0.5	1082.89	1.06776	-63.9	-114.1250	-0.847	-2438.81
1	1170.32	0.97506	87.4	156.1250	1.158	3336.33
1.5	1267.27	0.87228	97.0	173.1250	1.285	3699.61
2	1275.93	0.86309	8.7	15.4643	0.115	330.47

Gauge depth =

DP =

Top Perfs

Ps @ top perfs

Pressure gradient



÷

0.46 Psi/ft

Flowing





TIME [HR]

1400

Layering effect



12 X

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